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## PERSPECTIVE

# Asymmetric Electrode-Electrolyte Interfaces for High-Performance Rechargeable Lithium-Sulfur Batteries

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## Abstract

With a high cell-level specific energy and a low cost, lithium-sulfur (Li-S) battery has been intensively studied as one of the most promising candidates for competing the next-generation energy storage campaign. Currently, the practical use of Li-S battery is hindered by the rapidly declined storage performance during battery operation, as caused by irreversible loss of electroactive sulfide species at the cathode, dendrite formation at the anode and parasitic reactions at the electrode-electrolyte interface due to unfavorable cathode-anode crosstalk. In this perspective, we propose to stabilize the Li-S electrochemistry, and improve the storage performance of battery by designing asymmetric electrode-electrolyte interfaces that helps to simultaneously address the differentiated issues at both electrodes and facilitate charge transfer in the electrode/electrolyte and across the interfaces. The strategies discussed would shed lights on reasonable design of battery interfaces towards realization of high-performance Li-S batteries.

**Keywords:** Lithium-sulfur battery; Lithium metal anode; Sulfur cathode; Electrode-electrolyte interface

## 1. Introduction

Among advanced rechargeable batteries, Li-S battery has attained much attention in terms of being applied to emerging fields including grids and automobiles. It couples S cathode and Li metal anode, and both electrodes present theoretical specific capacities (S:  $1675 \text{ mAh}\cdot\text{g}^{-1}$ ; Li:  $3860 \text{ mAh}\cdot\text{g}^{-1}$ ), an order of magnitude higher than the electrode materials of traditional Li-ion batteries (e.g.,  $\text{LiFePO}_4$ :  $170 \text{ mAh}\cdot\text{g}^{-1}$  and graphite:  $372 \text{ mAh}\cdot\text{g}^{-1}$ ). As a result, the Li-S battery is capable to offer six times higher energy density than the Li-ion batteries (LIBs). Whereas, the practical application of Li-S battery is also hindered by both the challenges of S cathode and Li metal anode [1–4].

Different from intercalation-based lithium-ion batteries, S cathode follows a two-electron

conversion chemistry  $1/8\text{S}_8 + 2\text{Li} \leftrightarrow \text{Li}_2\text{S}$ . In the lithiation and delithiation reactions, the sulfur molecules would experience a stepwise transformation of solid-liquid-solid state. With high solubility, the intimate products, high-order polysulfides (e.g.,  $\text{Li}_2\text{S}_x$ ,  $x = 4-8$ ), tend to be dissolved in ether electrolyte, and shuttled from the cathode to the anode under the electric field, and finally deposited on the Li anode, which passivate the surface. Except for the dissolution and shuttle effect of LiPSs, the problems of insulative nature of S/Li<sub>2</sub>S and the huge volume change (80%) between S and Li<sub>2</sub>S would cause a continuous and rapid capacity fade, and emerge as roadblocks for the development of the S cathode. Remarkable approaches have been proposed to address the intrinsic shortcomings of S cathode toward practical applications, including optimization the

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structure of carbon materials, employment of catalysts, utilization of interfacial layer and modification of electrolytes, which are all investigated as important solutions to facilitate conversion kinetics of S cathode [5–10].

Although Li anode shows significant advantages in capacity ( $3860 \text{ mAh}\cdot\text{g}^{-1}$ ) and voltage ( $-3.042 \text{ V}$ ) over the conventional graphite anode materials, the generation of Li dendrites and dead Li during Li plating and stripping leads to the formation of unstable SEI and the accompanied low Coulombic efficiency. Hence, the Li metal anode is usually accompanied with serious safety problems and poor cycling performance, which impede the practical application of metal Li-based batteries. Significant efforts have been made to tackle the intrinsic problems of Li anode, including electrolyte additive, artificial SEI, superconcentrated electrolyte and solid-state electrolyte [11–19].

Interestingly, adoption of solid-state electrolyte has been considered as an effective method to restrain the dendrite growth and parasitic reactions on Li anode, but the reports concerning application of solid-state electrolyte on S cathode have less been mentioned [20–23]. Because solid electrolytes are unfavorable to the kinetics of sulfur, whereas liquid electrolytes with higher solubility and mobility of polysulfide could ensure faster redox reaction kinetics of sulfur [24]. Therefore, adopting the asymmetric interfaces which guarantees a liquid environment at S cathode and a solid environment at Li anode could simultaneously facilitate the electrochemical activity of cathode, restrict the shuttling and solve the dendrite problem of anode, and further promotes the advancement of practical Li-S battery.

## 2. Maintaining reactivity by selecting liquid electrolytes at cathode

The employment of liquid electrolyte at sulfur cathode benefits the solvation of the polysulfide and facilitates the reaction kinetics, but also aggravates the shuttling of polysulfide, which brings about low Coulombic efficiency and short cycling life [25]. The 1,3-dioxolane/1,2-dimethoxyethane (DOL/DME) ether electrolyte, as the most widely used solvent in Li-S batteries, presents moderate solvating capability for polysulfides, good sulfur utilization and fast reaction kinetics. A typical voltage profile with two plateaus of 2.3 V and 2.1 V is observed in DOL/DME-based solutions, which could be illustrated to a general reaction pathway of solid-liquid-solid multi-phase reaction of solid  $\text{S}_8$  to soluble  $\text{S}_x^{2-}$  and finally to solid  $\text{Li}_2\text{S}_2/\text{Li}_2\text{S}$  [26]. However, for practicable Li-S battery with low E/S

ratio (electrolyte/sulfur), several challenges appear in DOL/DME electrolyte, including higher viscosity and lower ionic conductivity, aggravated polysulfide shuttle and electrolyte solution depletion [27–29]. Therefore, other types of electrolyte solutions beyond conventional ether solution should be explored for Li-S cells with better performance.

A series of electrolytes such as high-concentration electrolyte, ionic liquids and hydrofluoroethers solvents have been introduced into Li-S battery. Different from DOL/DME electrolyte, these electrolytes can suppress the dissolution of polysulfides and have limited solubility of  $\text{Li}_2\text{S}_8$  (from 1 to  $100 \text{ mmol}\cdot\text{L}^{-1}$ ). Due to different solubilities of polysulfide, the sulfur reaction pathway and electrochemical performance could be significantly changed in comparison to the dissolution-precipitation mechanism in conventional electrolytes.

For high-concentration electrolyte, the interactions between the solvent and salt ions are comparatively stronger than that in  $1 \text{ mol}\cdot\text{L}^{-1}$  electrolyte, forming contact ion pairs (CIP) and aggregates (AGG) instead of plenty of free solvents [30]. Due to the lack of free-state solvent molecules, dissolution of polysulfide is restricted in high-concentration electrolyte, which could resolve the shuttling problem. In addition, high-concentration electrolyte shows other properties, which benefits the charge transfer, electrochemical stability, and battery safety, including high  $\text{Li}^+$  transference numbers, wide electrochemical windows and flame retardancy. However, low ionic conductivity and high viscosity are the key issues that restrain the electrochemical performance in cells with high-concentration electrolyte. To solve the problem, diluents with low viscosity could be introduced to form localized high-concentration electrolyte systems [31].

Nazar et al. [32] designed a electrolyte of  $(\text{ACN})_2/\text{LiTFSI}$  with the diluent of a hydrofluorinated (HFE), which could prevent the dissolution of polysulfide in the electrolyte, and ameliorate the common problems of poor Coulombic efficiency and capacity fading in Li-S battery. In contrast to conventional liquid electrolytes with disproportional coordination, this new electrolyte presents a different solvation structure without the existence of free solvent, that  $\text{Li}^+$  cations are closely surrounded by two ACN molecules. This structure renders the electrolyte negligible solubility and limits the mobility of polysulfide, which could enhance the sulfur utilization and further the overall electrochemical behavior (Fig. 1a). The ionic conductivity and viscosity of  $(\text{ACN})_2/\text{LiTFSI}/\text{HFE}$  are  $1.57 \text{ mS}\cdot\text{cm}^{-1}$  and  $8.6 \text{ cP}$ , respectively, which approach to those of DOL/DME solution.

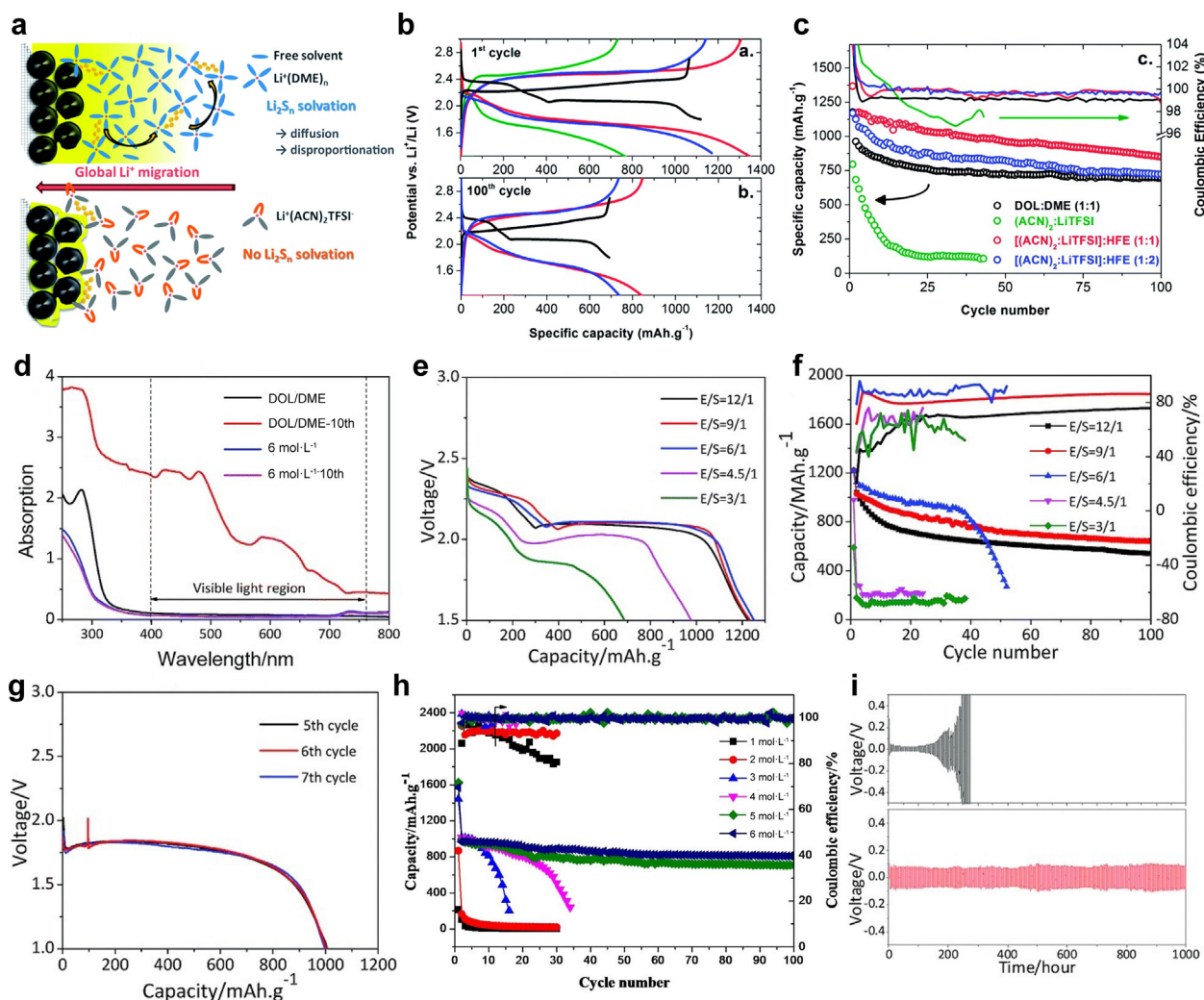


Fig. 1. (a) Schematic illustration of the migration of polysulfides in a Li-S battery with DME electrolyte and (I)<sub>2</sub>/LiTFSI electrolyte. (b) The initial and 100<sup>th</sup> galvanostatic discharge curve (GDC) voltage profiles in Li-S batteries at 0.2C with different electrolytes including DOL/DME (black), (ACN)<sub>2</sub>/LiTFSI (green), ACN/HFE(1:1) (red) aACN/HFE(1:2) (blue). (c) Cycling performance of different electrolytes in Li-S batteries for 100 cycles. Reproduced with permission of Ref. [32], copyright © 2014 RSC publishing. (d) UV-vis spectra of various electrolytes from the 10<sup>th</sup> cycle Li-S batteries. (e–f) GDC voltage profiles of Li-S batteries with varied E/S ratio(e) in 1 mol.L<sup>-1</sup> LiTFSI in DOL/DME electrolyte and (f) in HFME-6 mol.L<sup>-1</sup> carbonate electrolyte at 0.2C. (g) The self-discharge performance of HFME-6 mol.L<sup>-1</sup> carbonate during the 6<sup>th</sup> cycle after one-week storage. (h) Cycling performance of Li-S batteries with carbonate electrolyte of different concentrations at 0.2C. (i) Plating-stripping profile of symmetric Li-Li cells in 1 mol.L<sup>-1</sup> carbonate electrolyte and HFME-6 mol.L<sup>-1</sup> carbonate electrolyte (1 mA.cm<sup>-2</sup>, 1 mA.h.cm<sup>-2</sup>). Reproduced with permission of Ref. [33], copyright © 2013 RSC publishing.

The electrochemical behavior of Li-S battery with (ACN)<sub>2</sub>/LiTFSI/HFE is distinct from the two-plateau galvanostatic discharge curve in conventional Li-S battery, which shows a sloping curve without any clearly defined plateau (Fig. 1b). Due to the limitation of dissolution and shuttling of polysulfides, the capacity could reach to near the full theoretical capacity of 1373 mAh.g<sup>-1</sup>, and exhibit a specific capacity of 850 mAh.g<sup>-1</sup> after 100 cycles at 0.2 C (Fig. 1c). Although the low solubility of polysulfide would lead to cell polarization, the rate performance of Li-S battery with (ACN)<sub>2</sub>/LiTFSI/HFE is more excellent than that with DOL/DME, which delivers a discharge capacity of 900 mAh.g<sup>-1</sup> at 1 C.

Carbonate electrolytes have been widely used in lithium-ion batteries or metal lithium batteries but not in Li-S batteries, because they would have serious parasitic reactions with polysulfides. However, when the concentration of lithium salts is high to some extent, the side reactions between carbonate electrolyte and polysulfide could be suppressed [32]. Xiao et al. [33] proposed an ethylene carbonate/diethyl carbonate (EC/DEC) solution with 6 mol.L<sup>-1</sup> LiTFSI and hexafluoroisopropyl methyl ether (HFME) diluent, which enables the application of carbonate electrolyte in Li-S batteries. Due to high concentration environment of this new electrolyte, almost all carbonate molecules strongly coordinate with Li<sup>+</sup>,



which avoids the electrophilic carbon being attacked by polysulfides with high nucleophilic ability. Moreover, the slight amount of dissolved polysulfides would react with the carbonate molecules and form a protection layer on sulfur cathode, which impedes the further side reactions and dissolution of polysulfides. Thus, the high-concentration ester converts the ether-based Li-S batteries from non-rechargeable to rechargeable feature, showing a non-solvent behavior and akin solid-solid conversion. UV-Vis analysis is conducted to investigate the polysulfide solubility in DOL/DME and  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes before and after cycling, which turns out that no polysulfide is generated or solvated during cycling in the  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes (Fig. 1d). Different from the typical two-step voltage profile with dissolution-precipitation process, the  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes shows one-plateau curve and delivers a discharge capacity of  $1590 \text{ mAh}\cdot\text{g}^{-1}$  at 0.2 C. In addition, the Li-S batteries with  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes exhibit superior performance even at low E/S ratios while the batteries with DOL/DME shows high polarization and capacity decay at the E/S ratio less than 5:1 (Fig. 1e–f). This is because at low E/S ratios the transport of ions is influenced by the saturation of polysulfides in DOL/DME electrolyte, but the electrochemical properties of Li-S batteries with  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes only rely on the migration of  $\text{Li}^+$  ions. Surprisingly, the Li-S batteries with  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolytes present a zero self-charge behavior that the galvanostatic discharge curve of a cycled cell ideally remains the same even after one-week storage (Fig. 1g). In view of the property, a brilliant cycling performance is observed that the capacity retention is 83% after 100 cycles and the Coloumbic efficiency is close to 100% at a 0.2 C (Fig. 1h). Except for altering the sulfur reaction mechanism and preventing polysulfides, the high-concentration electrolyte could stably match the metal lithium anode. While the symmetric Li-Li cell with DOL/DME electrolyte presents a huge polarization after 150 h, and the cell with  $6 \text{ mol}\cdot\text{L}^{-1}$  EC/DEC/LiTFSI electrolyte could be cycled over 1000 h without significant voltage fluctuation or dendrite formation (Fig. 1i).

To achieve lower E/S ratio, a class of electrolytes with high-donor number (DN) or high-dielectric constant ( $\epsilon$ ) is adopted, which promotes the solubility of polysulfides and utilization of sulfur, such as dimethyl sulfoxide (DMA), dimethyl sulfoxide (DMSO), and 1-methylimidazole (MeIm) [34]. To model the solution environment in Li-S cells with high specific capacities,  $0.1 \times 10^{-3} \text{ mol}\cdot\text{L}^{-1}$  and

$1.6 \text{ mol}\cdot\text{L}^{-1}$   $\text{Li}_2\text{S}_6$  were added into four electrolytes to investigate the polysulfide solubility (Fig. 2a). In contrast to DOL/DME with insoluble residue at the bottom of bottles, DMA, DMSO and MeIm electrolytes could completely dissolve  $1.6 \text{ mol}\cdot\text{L}^{-1}$   $\text{Li}_2\text{S}_6$ , since highly polarizable solvent endows higher solubility for  $\text{Li}_2\text{S}_x$  species ( $x = 2,3,4,6,8$ ) than DOL/DME electrolytes. As for the electrolytes with  $1.6 \text{ mol}\cdot\text{L}^{-1}$   $\text{Li}_2\text{S}_6$ , the DMA and DMSO electrolytes show a clear blue color, which implies that  $\text{S}_3^-$  radical is the predominant species at low concentrations. The UV-Vis spectra also verify the high intensity of  $\text{S}_3^-$  radical in high DMA, DMSO and MeIm electrolytes (Fig. 2b). Whereas, the spectrum of DOL/DME electrolytes does not show the existence of  $\text{S}_3^-$  but a higher content of  $\text{S}_4^{2-}$ , indicative a different reduction pathway with high-DN electrolytes. This is because the  $\text{S}_3^-$  radical as a highly active intermediate could only be stabilized by high-DN electrolytes, and  $\text{S}_3^-$  radical creates a reaction pathway different from the pathway of  $\text{S}_4^{2-}$  in conventional electrolytes (Fig. 2c). According to reported study, the dissociation of  $\text{S}_6^{2-}$  to  $\text{S}_3^-$  is more preferable in high-DN electrolytes, and  $\text{S}_3^-$  could retard the surface passivation from solid  $\text{Li}_2\text{S}$  and accelerate the full output of capacity (Fig. 2d). For the sulfur cathode of  $2 \text{ mg}\cdot\text{cm}^{-2}$ , Li-S batteries with DMA and DMSO deliver an initial capacity of  $1250 \text{ mAh}\cdot\text{g}^{-1}$  while a cell with DME presents a capacity of  $1100 \text{ mAh}\cdot\text{g}^{-1}$  (Fig. 2e). When the loading amount of sulfur cathode is amplified to  $6 \text{ mg}\cdot\text{cm}^{-2}$ , the superiority of cell with DMA than cell with DME is more obvious (Fig. 2f). For batteries with DMSO or MeIm, the instability towards metal lithium anode is the key factor for bad electrochemical performance. Zhang et al. [35] proposed a high-DN electrolyte of tetramethylurea (TMU), which could simultaneously stabilize  $\text{S}_3^-$  and be compatible with metal lithium anode. The TMU/DOL electrolyte shows a high solubility of both  $\text{Li}_2\text{S}_8$  and  $\text{Li}_2\text{S}_4$ , while  $\text{Li}_2\text{S}_4$  is hardly dissolved in the DOL/DME electrolyte (Fig. 2g). The electrodeposition kinetics of lithium sulfide ( $\text{Li}_2\text{S}$ ) in TMU/DOL and DOL/DME electrolytes is also vastly different by chronoamperometric test. The different peaks in TMU/DOL could be explained by the reduction of  $\text{S}_3^-$ , which facilitates the deposition of  $\text{Li}_2\text{S}$  with smaller nucleus size and larger nucleation density (Fig. 2h) [36,37]. Equipping with carbon nanotube (CNT)/S composite cathode, Li-S battery with TMU realizes an initial discharge capacity of  $1134 \text{ mAh}\cdot\text{g}^{-1}$  with Couloumbic efficiency over 98% at 0.1C (Fig. 2i). Compared to the capacity of DME cell ( $943 \text{ mAh}\cdot\text{g}^{-1}$ ), the advantage of TMU cell is

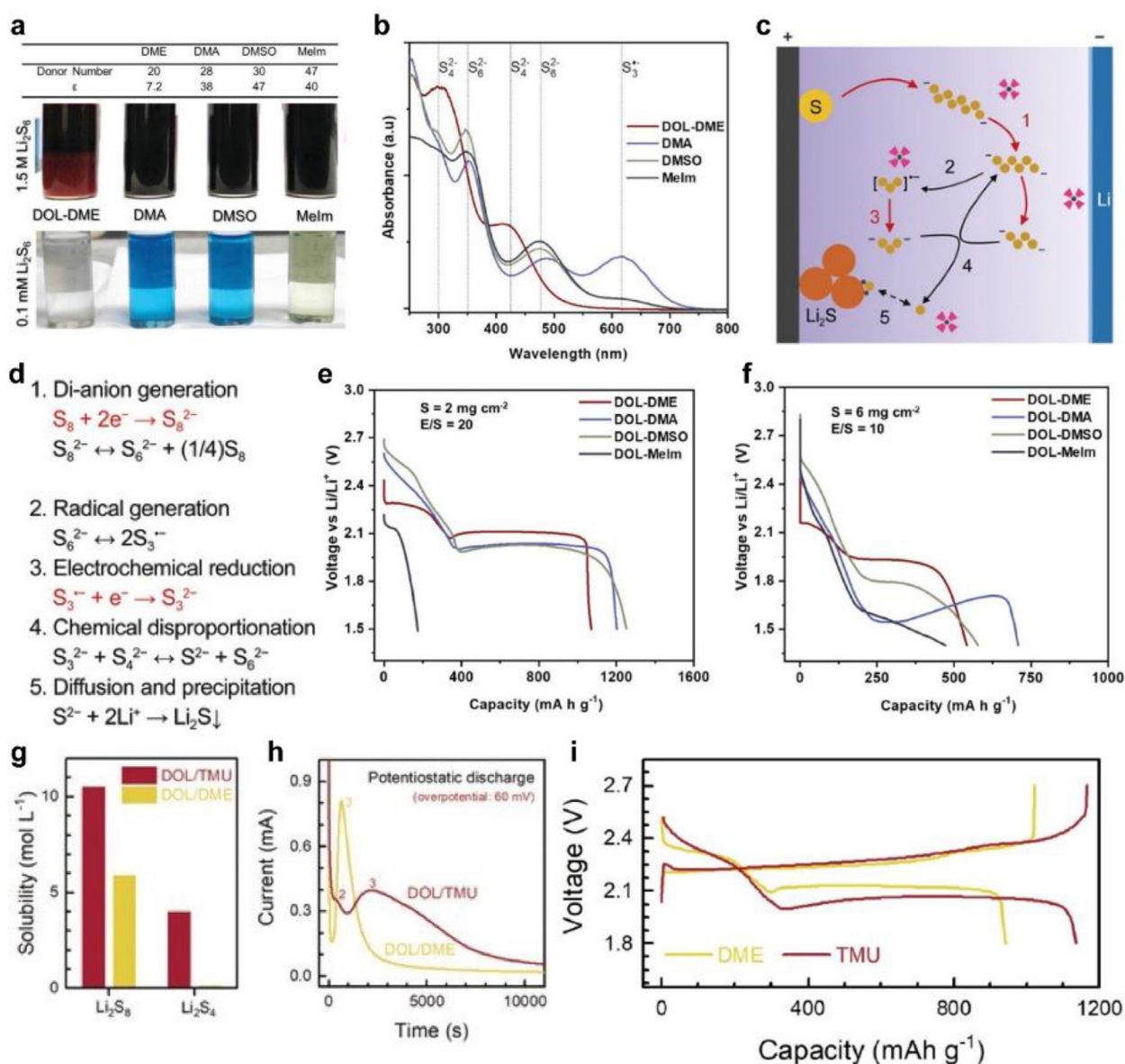


Fig. 2. (a) The table of DN and dielectric constant ( $\epsilon$ ) of the different solvents and optical images of solvents with  $1.5 \text{ mol}\cdot\text{L}^{-1}$  and  $0.1 \times 10^{-3} \text{ mol}\cdot\text{L}^{-1} \text{ Li}_2\text{S}_6$ . (b) UV-Vis spectra of DOL-DME, DMA, DMSO, and Melm electrolytes with  $0.25 \text{ mol}\cdot\text{L}^{-1} \text{ Li}_2\text{S}_6$ . Reproduced with permission of Ref. [34], copyright © 2018 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim. (c) Schematic illustration of the sulfur reaction pathway in a TMU-based electrolyte (Arrows: red solid: electrochemical reduction; black solid: chemical dissociation of  $S_6^{2-}$  into  $S_3^{\cdot -}$ ; black dashed: equilibrium of dissolution/precipitation). (d) polysulfide reaction pathway proposed by Cuisinier et al. Reproduced with permission of Ref. [35], copyright © 2018 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim. (e–f) First cycle discharge profiles with four different electrolytes and (e)  $2 \text{ mg}\cdot\text{cm}^{-2}$  and (f)  $6 \text{ mg}\cdot\text{cm}^{-2}$  sulfur cathode [34]. Reproduced with permission of Ref. [34], copyright © 2018 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim. (g) Solubility plots of  $\text{Li}_2\text{S}_8$  and  $\text{Li}_2\text{S}_4$  in DOL/TMU vs. in DOL/DME. (h) Chronoamperometric profiles in DOL/DME and DOL/TMU electrolytes. (i) Galvanostatic discharge-charge profiles of Li/CNT/S coin cells at 0.1 C in DME and TMU based electrolytes. Reproduced with permission of Ref. [35], copyright © 2018 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim.

reflected by the longer second plateau, which is attributed to an optimal pathway for  $\text{Li}_2\text{S}$  solvation and precipitation.

### 3. Restraining shuttling by introducing polymer electrolyte as blocking interlayer

Although the adoption of liquid electrolyte guarantees the electrochemical reactivity of sulfur

cathode, the shuttling of polysulfide and corrosion of lithium anode would pose challenges for the cycling performance of Li-S battery [38,39]. Therefore, introduction of polymer electrolyte as blocking interlayer could be effective solution. Ding et al. [40] designed a gel polymer electrolyte (GPE) composed of polyvinylidene fluoride (PVDF) and organo-polysulfide polymer (PSPEG), which could be permselective to  $\text{Li}^+$  and against

polysulfides. Sun et al. [41] proposed a conductive polypyrrole-coated Celgard, which could simultaneously immobilize polysulfides, and facilitate electron transportation and redox reactions on sulfur cathode. However, these strategies are based on an *ex-situ* synthesis, which results in an inferior interfacial contact between electrolyte and electrodes. Wang et al. [42] mentioned a strategy of gradient solidification, which could ensure a liquid environment at the sulfur cathode with rapid kinetics and an *in-situ* polymerized interface to suppress the shuttling. The solidifying interface is prepared by *in-situ* polymerization of DOL, which is initiated by the  $\text{LiPF}_6$  loaded on one side of the commercial PE separator towards the S cathode (Fig. 3a). During the battery assembly, the injected ether liquid electrolyte flows through the  $\text{LiPF}_6$  layer on the separator and triggers gelation of the electrolyte. Due to the slow diffusion in the gel electrolyte, the concentration of dissolved  $\text{LiPF}_6$  continuously to be declined from the separator to the cathode surface and to the bulk of the cathode, which accounts for different polymerization

degrees of DOL. As a result, a thin gradient solidification layer forms at the cathode/electrolyte interface (Fig. 3b). The liquid electrolyte is maintained in the bulk of cathode to enable wetting of S by liquid electrolyte for high electrochemical activity. On the other hand, the surface of separator is highly solidified, which effectively inhibits the dissolution and shuttle of polysulfides, and improves the cycling performance of cell. The chemical species along the gel electrolyte were detected and visualized by time-of-flight secondary ion mass spectrometry (ToF-SIMS), showing a continuous increment of the  $\text{Li}^-$ ,  $\text{F}^-$ , and  $\text{P}^-$  signals from the surface (at the cathode side) to the bulk of the gel (Fig. 3c). According to the intensity of representative signals, the concentration in the bulk of gel electrolyte is  $1.5 \text{ mol} \cdot \text{L}^{-1}$  and the concentration of the gel surface is around  $0.15 \text{ mol} \cdot \text{L}^{-1}$ , implies that only a minute amount of salt could reach the bulk of the cathode and cannot introduce the gelation process (Fig. 3d). As shown in Fig. 4G–H, the prepared  $\text{LiPF}_6$ -supported separator strips could be easily rolled up without

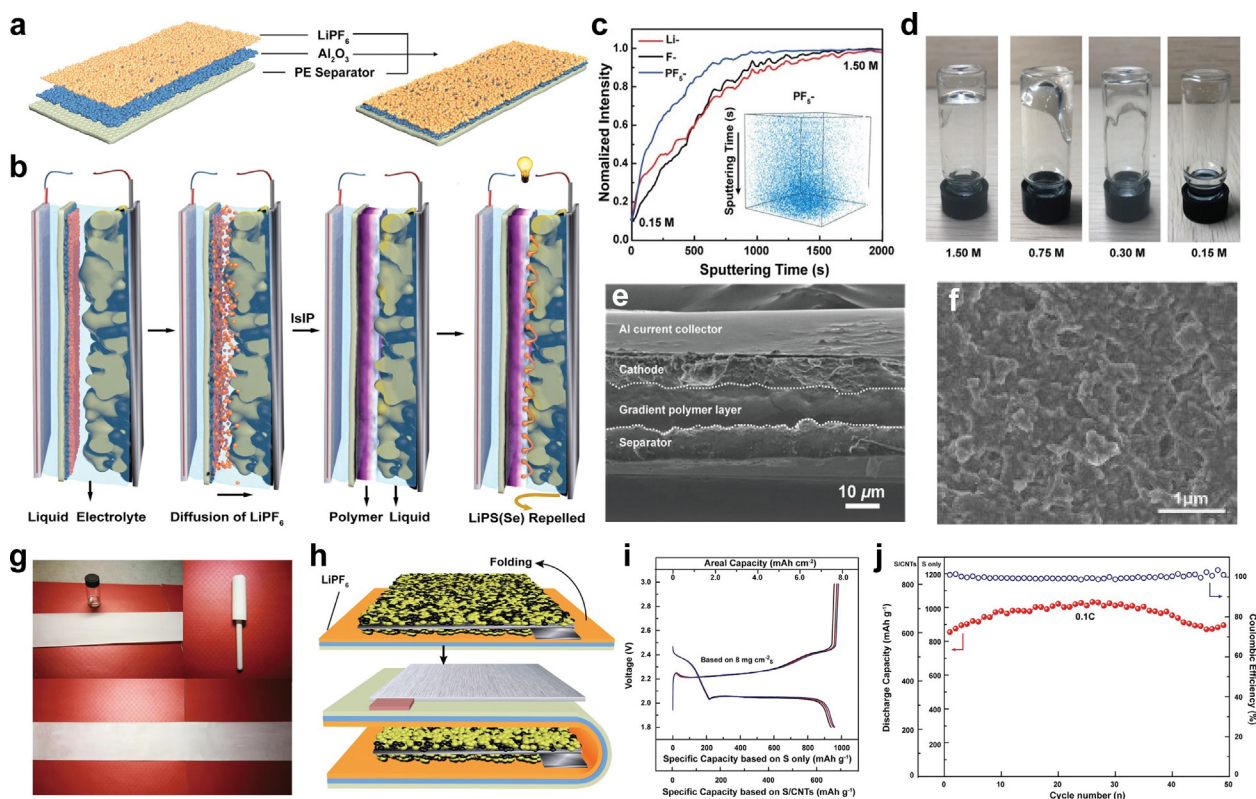


Fig. 3. (a) Structure of the  $\text{LiPF}_6/\text{Al}_2\text{O}_3/\text{PE}$  separator. (b) Schematic illustration showing the *in-situ* interfacial polymerization of liquid electrolyte realized with the  $\text{LiPF}_6/\text{Al}_2\text{O}_3/\text{PE}$  separator. (c) TOF-SIMS depth profiles obtained from the gel polymer interlayer on the separator, in which the inset shows the 3D spatial configuration of  $\text{PF}_5^-$  signal. (d) Optical images showing the various polymerization degrees of liquid electrolyte with different  $\text{LiPF}_6$  concentrations. (e) Cross-sectional SEM image illustrating multilayered structure of the Li-S full battery. (f) SEM image of sulfur cathode surface after the polymerization having been finished. (g) Optical images showing the preparation process of the  $\text{LiPF}_6/\text{Al}_2\text{O}_3/\text{PE}$  separator roll. (h) Schematic illustration of the steps for the assembly of Li-S pouch cells. (i) GDC voltage profiles and (j) cycling performance of the assembled Li-S pouch cell at 0.1C. Reproduced with permission of Ref. [42], copyright © 2020 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim.



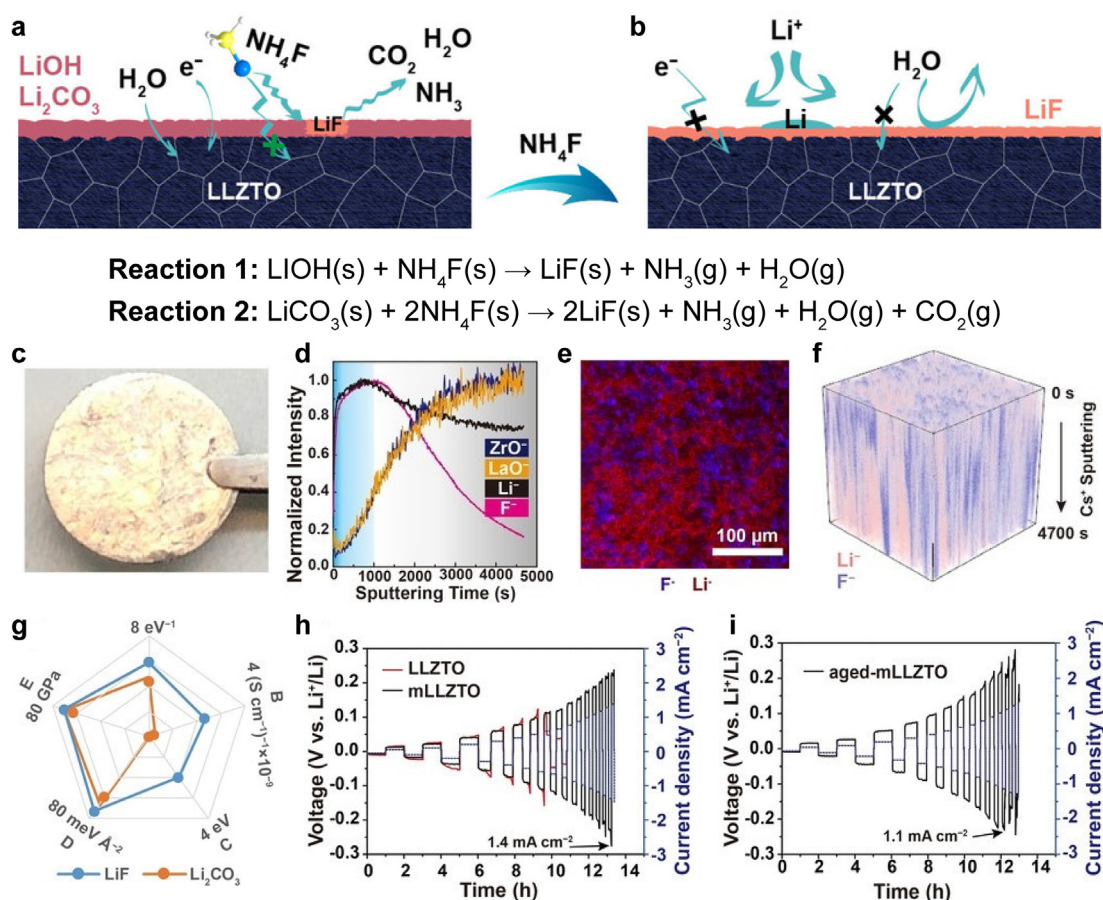


Fig. 4. (a) Schematic illustration showing the formation of LiF-coated LLZTO by  $\text{NH}_4\text{F}$  treatment. (b) The surface stability of LiF-coated LLZO against air exposure, electron and hostless evolution of Li metal; (c) Optical image of the wetting behavior of molten Li on mLLZTO. (d) Depth profiles of  $\text{ZrO}^-$ ,  $\text{LaO}^-$ ,  $\text{Li}^-$  and  $\text{F}^-$  signals at the Li/mLLZTO interface. High-resolution (e) 2D/ (f) 3D maps of  $\text{Li}^-$  and  $\text{F}^-$  signals at the Li/mLLZTO interface. (g) Comparison of LiF and  $\text{Li}_2\text{CO}_3$  in various physical and chemical properties; A: 1/surface diffusion barrier energy; B: 1/electronic conductivity; C: electron tunnelling barrier; D: interfacial energy; E: bulk modulus. (h) Galvanostatic Li plating/stripping voltage profiles at step-increased current densities of Li/Li symmetric cells assembled with the LLZTO and mLLZTO pellets. (i) Galvanostatic Li plating/stripping voltage profiles at step-increased current densities of Li/Li symmetric cells assembled with the mLLZTO pellets after being aged in the air for 2 days. Reproduced with permission of Ref. [50], copyright © 2020 WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim.

any exfoliation of  $\text{LiPF}_6$  powder and the pouch cell adopted a typical “Z stacking” configuration. The battery with new separator delivers a high initial capacity of  $1100 \text{ mAh} \cdot \text{g}^{-1}$  and a reversible capacity of  $1000 \text{ mAh} \cdot \text{g}^{-1}$  at 0.1C, and a reversible capacity of around  $900 \text{ mAh} \cdot \text{g}^{-1}$  at 0.5C, even at a high S mass content of 70%. By using the strategy, a practical Li-S pouch cell was assembled, which delivered a high reversible capacity of  $950 \text{ mAh} \cdot \text{g}^{-1}$  and a lifespan of 50 cycles at a high S mass loading of  $8 \text{ mg} \cdot \text{cm}^{-2}$  (Fig. 3i–j).

#### 4. Suppressing dendrites by adopting solid-state electrolytes at anode

To address the dendrite issue in Li-metal batteries, ceramic solid electrolytes, such as cubic garnet-type LLZO or its derivatives, have been regarded as one of the most promising solutions

[43–46]. It simultaneously features many advantages, including high  $\text{Li}^+$  conductivity, high  $\text{Li}^+$  transference number, wide electrochemical window of 0–6 V, and high shear modulus and high compactness, which are beneficial to inhibit dendrite evolution and stabilize the Li/electrolyte interface. However, the garnet itself shows poor chemical stability against water and carbon dioxide in the ambient air. Once been exposed in the air, many Li-containing contaminants, including lithium hydroxide and Lithium carbonate, would be generated on the garnet surface, which show low Li-ion conductivity and poor wettability against Li metal (Fig. 4a). Thus, these surface contaminants may easily trigger dendrite nucleation and formation at the interface, so they are supposed to be removed by strong acid or high-temperature sintering [47–49].



To improve the chemical stability against air exposure, Duan et al. [50] developed a simple and moderate-temperature chemistry to convert the contaminants into a fluorinated nanocoating layer on the surface of the garnet particles (Fig. 4b). According to the theory that ammonia fluoride is capable to react with lithium hydroxide and lithium carbonate, the LiF-coated garnet-type LLZTO pellets were prepared by the treatment with  $\text{NH}_4\text{F}$ . The treated LLZTO pellet was not contaminated even after being aged in ambient air for a few days. This is because of the hydrophobic nature from the fluorinated garnet surface, which prevents the contaminant-generating parasitic reactions between LLZTO and moist in the air. By being dipped into molten Li, a uniform garnet layer could intimately coat on the surface of Li metal (Fig. 4c). TOP-SIMS results show that the  $\text{ZrO}^-$  and  $\text{LaO}^-$  signals representing the LLZTO are gradually increased, but the  $\text{F}^-$  signal firstly remains stable and later quickly diminishes (Fig. 4d). With the proof of 2D and 3D configurations of  $\text{F}^-$  and  $\text{Li}^-$  signals, it can be seen that LiF nanocoating on mLLZTO remains stable during the formation of Li/garnet interface.

Considering that LiF has a lower barrier energy for diffusion of  $\text{Li}^+$  on the surface (0.17 eV) and a higher electron tunnelling barrier (2 eV) than those of  $\text{Li}_2\text{CO}_3$  (0.23 eV and 0 eV, respectively), the fluorinated interface helps to form smooth and compact deposits rather than typically rough and dendritic morphology even at high current densities (Fig. 4g). In addition, the  $\text{Li}^+$  diffusivity at an electrode/electrolyte interface plays a key role in controlling the critical current density, so that the modified interface could enable the regulated Li plating/stripping at a high  $\text{Li}^+$  flux and achieve a prolonged cycling of Li/Li symmetric cells at a high critical current density of  $1.4 \text{ mA}\cdot\text{cm}^{-2}$  (Fig. 4h). After air exposure, the LLZTO pellet still keeps high critical current density of  $1.1 \text{ mA}\cdot\text{cm}^{-2}$  (Fig. 4i).

Although the adoption of garnet electrolyte could suppress the Li dendrite, it is difficult to apply conventional manufacture techniques to prepare ceramic oxide electrolyte pellets with thickness of  $<200 \mu\text{m}$  due to the inherently brittle nature of garnet electrolyte property. Furthermore, the ceramic pellet does not have adequate “softness” to accommodate the deformation strains caused by the volume change of electrode materials during  $\text{Li}^+$  plating/stripping. Nevertheless, the garnet powder does not support fast interparticle  $\text{Li}^+$  conduction at loosely-packed grain/particle boundaries. Therefore, adopting solid composite electrolytes especially with thin-film polymer could be effective

solution towards the pathway to a practical solid-state Li-metal battery [46,51].

Chen et al. [52] introduced a uniform polyacrylonitrile nanocoating on the surface of LLZTO garnet particles by high-energy ball-milling. The cross-sectional SEM image shows that the total thickness of the solid electrolyte layer is  $<10 \mu\text{m}$  (LLZTO@PAN  $8 \mu\text{m}$  and PEO  $1 \mu\text{m}$ ), which meets the requirements for building LMBs with competitive energy density (Fig. 5a). It is also noted that the LLZTO@PAN particles could permeate into both the LFP layer and the PEO electrolyte layer, which is beneficial for facilitating  $\text{Li}^+$  conduction at heterointerfaces. The modified garnet powder shows an ultrahigh mass content of ceramics of 94.3% and a polymer coating with a thickness of 7 nm, which ensures efficient interparticle  $\text{Li}^+$  transport without pellet sintering or applying external pressure. According to the FTIR and NMR spectra, the coupling between DMSO and LLZTO leads to dehydrocyanation of PAN on the garnet surface and formation of conjugated structures in the polymer phase. According to DFT calculations, dehydrocyanated PAN shows enhanced interaction with the garnet surface with strong electron transfer, and a space charge layer is formed at the garnet/polymer interface, which contributes to faster interfacial  $\text{Li}^+$  exchange. In addition, because the thickness of the polymer coating falls into the same scale as the space charge layer and the conjugated region, Li ions are easily and rapidly transported between two adjacent ceramic particles through the polymer phase (Fig. 5b). The interparticle lithium conduction mechanism is further testified by solid-state NMR measurement. The 2D  $^1\text{H}$ - $^7\text{Li}$  heteronuclear correlation spectrum indicates that the Li ions dissociated from LiTFSI are trapped by the  $\text{C}=\text{C}$  bond possibly because of the high electron density (Fig. 5c). Meanwhile, 2D  $^7\text{Li}$ - $^7\text{Li}$  exchange spectrum indicates fast  $\text{Li}^+$  exchange at the garnet/polymer interface (Fig. 5d). With PAN providing the  $\text{Li}^+$  transport channels between the garnet particles, thin-film electrolytes with a thickness of less than  $10 \mu\text{m}$  can be prepared from the LLZTO@PAN powder via tape-casting directly on the cathode surface. The composite solid electrolyte exhibits a high ionic conductivity of  $1.1 \times 10^{-4} \text{ S}\cdot\text{cm}^{-1}$  at  $60^\circ\text{C}$  with an activation energy of 0.36 eV, indicating an improved wetting of PAN on LLZTO and a low energy barrier for  $\text{Li}^+$  diffusion (Fig. 5e). Also, the electrolyte presents a high  $\text{Li}^+$  transference number of 0.66, which is favorable for restricting the growth of dendrite during the plating/stripping of Li metal (Fig. 5f). Assembled with the electrolyte, the Li/LFP all-

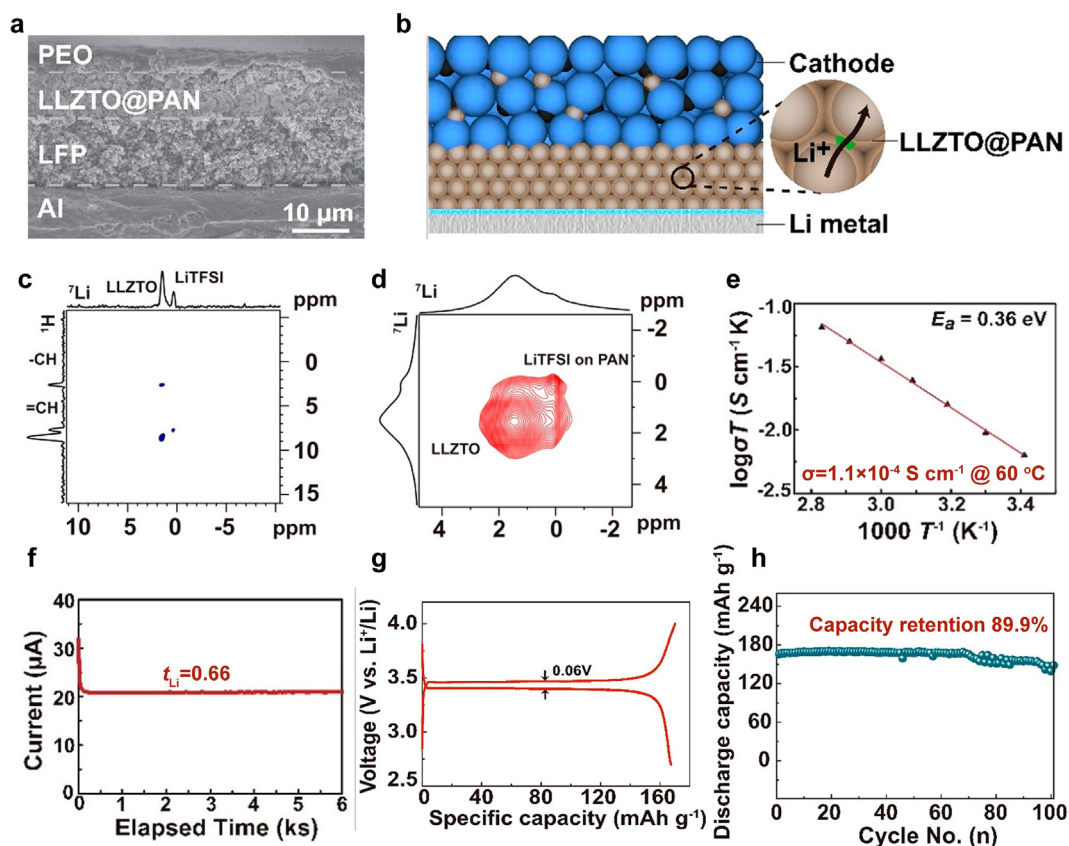


Fig. 5. (a) Cross-sectional SEM image LLZTO@PAN and PEO electrolyte layers on the cathode; (b) Schematics showing different  $\text{Li}^+$  transport mechanisms through the ceramics/polymer interface; (c) 2D Solid-state NMR  $^7\text{Li}$ - $^1\text{H}$  HETCOR spectra of LLZTO@PAN at 298 K. (d) 2D Solid-state NMR  $^7\text{Li}$ - $^7\text{Li}$  HETCOR spectra of LLZTO@PAN at 298 K. (e) Arrhenius plot of LLZTO@PAN at varied temperatures; (f) Chronoamperometric profile of a symmetric Li/Li cell with the LLZTO@PAN electrolyte; (g) Charge-discharge voltage profile at 0.1C of Li/LFP cell with the LLZTO@PAN electrolyte (h) Cycling performance of the Li//LLZTO@PAN/PEO/LFP cell at 60 °C at 0.1C. Reproduced with permission of Ref. [51], copyright © 2021 American Chemical Society.

solid-state cell delivers a high reversible capacity of  $167 \text{ mAh} \cdot \text{g}^{-1}$  at 0.1C with a small polarization of 0.06 V (Fig. 5g), and achieves a capacity retention of 89.6% after 100 cycles (Fig. 5h).

In addition to oxide electrolytes, sulfide electrolytes and organic-inorganic composite electrolytes have also been used to suppress Li dendrites. Wang et al. [53] improved the interfacial contact and charge transfer stability between sulfide electrolyte and Li metal anode by applying a LiF-rich *in-situ* solidified  $\text{Li}^+$ -conductive interlayer, leading to inhibition of electrolyte decomposition and dendrite-free Li plating/stripping at the interface. Chen et al. [54] designed a composite electrolyte with fast ion-conducting ceramic nanofiller and functional polymer skeleton, which enable a dendrite-free Li surface after cycling.

## 5. Conclusions

For practical application of Li-S batteries, a series of problems should be solved, including the dissolution/shuttle of LiPSs, the sluggish interfacial

charge transfer, the damage of cathode bulk structure and uncontrollable Li dendrite growth. In view of different situations at cathode and anode sides, asymmetric electrode/electrolyte interfaces should be constructed. To conclude, this review discusses types of strategies at cathode, separator and anode sides in the Li-S battery. From a practical point of view, an ideal Li-S battery should take into account high energy density and long cycle life, which requires that the electrolyte could optimize the electrochemical reactivity of sulfur, prevent the shuttling of polysulfide and stabilize the metal lithium anode. Accordingly, a liquid electrolyte should be used inside cathode to ensure fast  $\text{Li}^+$  transport, a gel electrolyte should be used on cathode side to achieve good interfacial contact and inhibit polysulfide shuttle, and a solid-state electrolyte should be used on anode side to suppress Li dendrites. By purposely selecting suitable strategies at the corresponding domain and building asymmetric interfaces, we would obtain a high-performance and practical Li-S battery.

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## 面向高性能锂-硫二次电池应用的非对称电极-电解质界面

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### 摘要

锂-硫电池具有高的理论电芯比能量和低成本, 是极具应用前景的下一代电化学储能技术, 已被广泛研究。实用化锂-硫电池技术目前面临的挑战主要包括正极侧电活性硫物种在充放电过程中的不可逆损失, 负极侧枝晶形核生长, 以及因活性硫迁移至负极而导致的界面副反应, 上述问题会导致电池工况条件下性能迅速衰退, 引发电池失效和安全问题。本工作中, 我们提出通过设计非对称的电极-电解质界面稳定锂-硫电池正负极电化学, 协同促进电极/电解质体相和界面电荷输运, 从而延长电池循环寿命, 显著提升电化学性能。本文所讨论的策略有望指导电池界面理性设计, 助力实现高性能的锂-硫电池。

**关键字:** 锂-硫电池; 锂金属负极; 硫正极; 电极-电解质界面